Journal of King Saud University - Science 35 (2023) 102863

Contents lists available at ScienceDirect

### Journal of King Saud University – Science

journal homepage: www.sciencedirect.com

Original article

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# Utilization of triethylammonium hydrogen sulphate-mediated solvent for optimization of asiaticoside extraction and antioxidant capacity of *Centella asiatica (L.)*



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#### ARTICLE INFO

Article history: Received 12 January 2023 Revised 5 April 2023 Accepted 23 August 2023 Available online 26 August 2023

Keywords: Triethylammonium hydrogen sulfate Asiaticoside Phenolic compounds Antioxidant Optimization

#### ABSTRACT

Asiaticoside, a pentacyclic triterpene of *Centella asiatica* with broad pharmacological actions. Higher asiaticoside content of Centella extracts in food products increases their nutritional and medicinal values. Protic ionic liquids (PIL) were utilized as bioactive extraction additives. The research focuses on obtaining the optimum extraction parameters for higher asiaticoside yield, and Centella extract antioxidant capacity. Optimization of all responses (asiaticoside yield, TPC, TEAC) achieved through faced-centered composite design (FCCD) involving three factors (temperature, extraction time, and triethylammonium hydrogen sulfate, [TEA][HSO4] %). The optimal conditions were 66 °C, 12 h duration, and 20% [TEA] [HSO4], which resulted in 4.44  $\pm$  0.05% (w/w) asiaticoside, TPC of 114.11  $\pm$  12.58 mg GAE /g and TEAC of 70.01  $\pm$  5.74 µmol TE/g respectively. All responses fit the quadratic model with proximity between predicted and experimented values. Procurement of higher asiaticoside yield, TPC, and TEAC verified for higher bioactive extractions. Research expansion by utilizing other PILs for plant extraction in addition to solute–solvent interaction study will be beneficial for the designation of an efficient plant extraction process that maximizes the plant-based product market.

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#### 1. Introduction

*Centella asiatica* (L.) or locally known as "Pegaga" in Malaysia, is a prominent therapeutic herb with multiple pharmacological actions (Jhansi and Kola, 2019; Wong and Ramli, 2021) such as anti-inflammatory, antioxidant, wound ameliorating, neuroprotective (Yadav, 2021), antimicrobial, anti-diabetic, antifungal, and anticancer properties (Tripathy and Srivastav, 2023; Tripathy

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et al., 2022). These benefits contributed by flavonoids and terpenoids content such as asiatic acid, madecassoside, and asiaticoside (Fig. 1). Commercially, there were more than 100 Centella-based formulations in the market with at least 2% asiaticoside and madecoside content required for the product benefits (Idris and Mohd Nadzir, 2021; Prasad et al., 2019).

Therefore, the extraction processes parameters such as solvent concentration, pH, temperature, and extraction duration are crucial in obtaining the bioactive compounds (Kumar et al., 2021; Sridhar et al., 2021). Ethanolic extraction has been widely employed for *C. asiatica* leaves extraction (Idris and Mohd Nadzir, 2021; Monton et al., 2019; Thong-On et al., 2021; Yingngam et al., 2020). The asiaticoside yield through ethanol-based extraction reportedly ranged from 0.09% to 0.193% (Monton et al., 2019). Other studies reported the optimum conditions for polyphenols extraction from Centella to be 37% ethanol concentration at 70.2 °C and 110.5 min (Mohapatra et al., 2021). Even at optimum conditions reported, the asiaticoside yield was still low than the minimum requirement.

https://doi.org/10.1016/j.jksus.2023.102863

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Fig. 1. Chemical structure of [TEA][HSO<sub>4</sub>] and asiaticoside.

Ionic liquids (ILs) efficiency as green solvents for bioactive extraction attracts attention (Choi and Verpoorte, 2019; Ferreira et al. 2022; Lim et al., 2022; Yansheng et al., 2011). Protic ionic liquids (PILs) are a subgroup of IL that are non-volatile, nonflammable, and more stable at higher temperatures than conventional organic molecular solvents (Clough et al., 2015; Greaves and Drummond, 2015; Nasirpour et al., 2020). Triethylammonium hydrogen sulfate, [TEA][HSO<sub>4</sub>] (Fig. 1) is one of the PILs that has received increasing attention due to its ultra-low-cost that can be made at bulk scale for \$1.24 kg<sup>-1</sup>, favorably comparable to acetone (Chen et al. 2014). [TEA][HSO<sub>4</sub>] effectively deconstruct various types of biomass by providing dual functions: (1) a Brønsted acid catalyst that disrupts chemical linkages in biomass complex structure and: (2) a delignifier that dissolves lignin (Khan et al., 2020; Welton, 2013; Zahari et al., 2018). Due to this, it is plausible to destruct the plant tissues and cell walls of C. asiatica, increasing their permeability and consequent molecular diffusion, playing a crucial role in higher extraction yield (Zhao et al., 2014). Moreover, asiaticoside was reportedly more stable in acidic pH (Puttarak et al., 2016).

There has yet to be the utilization of [TEA][HSO<sub>4</sub>] reported for Centella extraction, and using previous research optimum parameters at different operational conditions is not plausible. Hence, this study investigated the optimum extraction condition for asiaticoside yield and antioxidant capacity by utilizing [TEA][HSO<sub>4</sub>] as a co-solvent in the *C. asiatica* leaves extraction, aiding by response surface methodology (RSM).

#### 2. Methodology

#### 2.1. Preparation of Triethylammonium hydrogen Sulfate, [TEA][HSO<sub>4</sub>] IL

The synthesis followed a method published elsewhere (Salahi et al. 2016; Wang et al., 2006; Zahari et al., 2018). 2.5 M of

H<sub>2</sub>SO<sub>4</sub> (98 g, 1 mol) was added dropwise to triethylamine, N<sub>222</sub> (101 g, 1 mol) over 1 h at 60 °C. The mixture continued to be stirred at 70 °C for 1 h. Water traces were removed under pressure at 80 °C. The as-synthesized [TEA][HSO<sub>4</sub>], obtained as a colorless solid, was characterized by 1D-NMR (see Fig. S1 in ESI† for <sup>1</sup>H and <sup>13</sup>C NMR spectra) (ppm): <sup>1</sup>H NMR (DMSO *d*<sub>6</sub>): 1.16 (t, 9H, 7.4 Hz), 3.06 (q, 6H, 7.4 Hz), 9.26 (s, 1H); <sup>13</sup>C NMR (DMSO *d*<sub>6</sub>): 9.02 (CH<sub>3</sub>) and 46.05 (CH<sub>2</sub>).

#### 2.2. Asiaticoside extraction from Centella asiatica

*Centella asiatica* leaves were collected in Negeri Sembilan, Tampin, Malaysia. They were cleaned, dried in an oven for 24 h at 30 °C, and ground into a particle size of 0.5 mm. A binary solvent system was first prepared by mixing [TEA][HSO<sub>4</sub>] and EtOH-40% according to the desired ratio Table 1. The mixture at 10 ml/g ratio was incubated at a specific period. The asiaticoside yield in the collected extract was quantified using reverse phase-high performance liquid chromatography (RP-HPLC).

#### 2.3. Quantification of asiaticoside yield (AY)

The extract was diluted with deionized water at a 1:1 ratio, filtered using a 0.22 mm nylon syringe filter, and analyzed on a Shimadzu LC-20 with a photodiode array detector (PDA) at 220 nm and a C-18 column. The following conditions were used: 0.8 ml/min flow rate, 20  $\mu$ l injection volume, methanol, and deionized water (70/30 (vol/vol)) as mobile phase and column temperature of 30 °C. Standards asiaticoside solution prepared in deionized water at concentrations ranging from 10 to 100 ppm (see Fig. S2 in ESI† for the calibration curve).

#### 2.4. Measurement of total phenolic content (TPC)

Diluted extracts (1 mg/ml, 20  $\mu$ l of each sample) were placed in microplate wells. Subsequently, the wells were left for 10 min in the dark at room temperature after the addition of 10 v/v%, 100  $\mu$ l Folin Ciocalteu reagent, followed by Na<sub>2</sub>CO<sub>3</sub> (7.5%, 80  $\mu$ l) addition to each sample. After 2 h left in the dark, the mixture absorbance was read at 765 nm. Gallic acid calibration curve plot (see Fig S2 in ESI†) aids TPC quantification in mg gallic acid equivalents (GAE) unit per g of dried extract.

#### 2.5. Trolox equivalent antioxidant capacity (TEAC) quantification

DPPH scavenging ability measures the DPPH radicals quantity scavenged by phenolic compounds (ArOH) in the extract. Neutralization of DPPH radical in the assay occurred by accepting hydrogen atom or electron from antioxidant species, resulting in reduced DPPH (DPPH-H) (Bibi Sadeer et al., 2020), as shown in Eq. (1). The extracts (100  $\mu$ l) and 0.2 mM of DPPH solution (100  $\mu$ l) were pipetted into a 96-well plate. The absorbance was read at 517 nm after 30 min dark incubation. Equation (2) was used to determine DPPH radical scavenging %. TEAC represented the antioxidant activity in  $\mu$ mol TE/g and was calculated using

Table 1	
Physical properties of [TEA][HSO <sub>4</sub> ]: EtOH binary solvent systems.	

[TEA][HSO4] /EtOH ratio (g/ml)	%[TEA] [HSO <sub>4</sub> ]	Viscosity (Pa.s)	рН
0.25	20	0.0037 ± 0.0001	1.20 ± 0.012
0.66	40	$0.0081 \pm 0.0006$	1.27 ± 0.006
1.0	50	0.0116 ± 0.0007	1.37 ± 0.042
1.5	60	$0.0189 \pm 0.0000$	1.39 ± 0.010

DPPH scavenging activity of trolox (%) against the log series concentration calibration curve (see Fig. S2 in ESI†).

$$DPPH^* + ArOH DPPH-H + ArO^*$$
(1)

DPPH scavenging 
$$\% = [(A_{DPPH} - A_{extract})/A_{DPPH}] \times 100$$
 (2)

#### 2.6. Optimization through response surface methodology (RSM)

RSM allowed the analysis of multiple factor effects and their interactions towards response variables (Pais-Chanfrau et al., 2021). Thus, more information can be obtained from a limited number of experiments (Goren et al. 2022). Twenty experimental trials were performed per Face-centered composite design (FCCD) with temperature, X<sub>1</sub> (30 °C,55 °C, 80 °C), extraction time, X<sub>2</sub> (12 h,18 h, 24 h), and [TEA][HSO<sub>4</sub>] %, X<sub>3</sub> (20%, 40%, 60%) as variables, while, AY, TPC, and TEAC as responses. Design Expert 13 was used as a statistical tool for the experimental design and analysis. The FCCD consists of six axial points, eight factorial points, and one center with six replications.

#### 3. Discussion

#### 3.1. Time course extraction and experimental output

We monitored the asiaticoside yield (AY) in designing the conditions for RSM. As a control, the ground leaves were soaked in EtOH-40% at 65 °C for 1 h, yielding  $0.28 \pm 0.02\%$ w/w of asiaticoside. [TEA][HSO<sub>4</sub>]/EtOH (1 g/ml) addition significantly enhanced the AY by 9 times ( $2.5 \pm 0.27\%$ w/w). Hence, time course extraction under the same conditions was performed. Fig. 2 shows that the AY increases significantly up to 12 h and then plateaus thereafter, which can be explained by Fick's second law of diffusion (Benchikh et al., 2021).

Overall, the twenty experimental trials gave the following responses: AY ranging from 2.75.% to 4.75% (w/w); TPC of 18.98 to 112.58 mg GAE/g, and; TEAC of 29.28 to 72.05  $\mu$ mol TE/g. All responses adequately fitted quadratic polynomial equations, as indicated by a significant model, non-significant Lack-of-fit test, and R<sup>2</sup> values higher than 0.75 (Table 3).

#### 3.2. Independent variable effects on responses

According to the analysis of variance (ANOVA) in Table 4 (Entry 1–3), all independent variables were significant towards AY. For TPC and TEAC, extraction temperature had a non-significant individual effect, while the other variables were significant.

Temperature showed a positive coefficient towards AY (Table 4, Entry 1), as depicted by Run 4 *versus* Run 10 (Table 2). Generally, secondary metabolites are secluded within the cell wall. Higher temperature aid in cell wall destruction, releasing abundant bioactive compounds (Gómez-Maqueo et al., 2020). Meanwhile, extraction time and [TEA][HSO<sub>4</sub>]% exhibited a negative coefficient toward all responses (Table 4, Entry 2, Entry 3). This indicates that longer extraction time (Table 2, Run 1 *versus* Run 7) and an increase in [TEA][HSO<sub>4</sub>] % (Table 2, Run 2 *versus* Run 4) led to a decrement in responses. Polyphenols degradation at extended extraction duration at high temperatures (Kim et al., 2018) and high viscosity of the binary solvent (Table 1) leading to mass transfer limitations (Fuad and Nadzir, 2023) explained this occurrence.

#### 3.3. Independent variables interactions

AY does not significantly influence by all independent variables interactions (Table 4, Entry 4–6). In contrast, TPC was positively impacted by the interaction of [TEA][HSO<sub>4</sub>]% with temperature and extraction time ( $X_1X_3$ ;  $X_2X_3$ ) (Table 4, Entry 5 and 6). Extended extraction time aid in leaching the bioactive compound out into the solvent system, resulting in higher TPC (More and Arya, 2021; Sharma and Dash, 2021). Meanwhile, only positive interaction of temperature-[TEA][HSO<sub>4</sub>] % ( $X_1X_3$ ) was observed for TEAC (Table 4, Entry 5). This occurrence is plausibly due to lower solvent viscosity with temperature increment, enhancing the bioactive mass transfer into the solvent system (Yusoff et al., 2022).

The variable interactions on TPC and TEAC were further visualized in 3D-surface plots, as shown in Fig. 3. In Fig. 3 (a), at 55 °C, the highest TPC was given when variables  $X_2$  and  $X_3$  had the smallest value. This suggests that lower [TEA][HSO<sub>4</sub>] % and shorter extraction time favor higher TPC value.

Fig. 3 (b) shows a TPC response of  $X_1$  versus  $X_3$  at 18 h. The plot proposes that lower [TEA][HSO<sub>4</sub>] % and moderate temperature leads to higher TPC value. Similar patterns were observed for the TEAC response of  $X_1$  versus  $X_3$  at 18 h (Fig. 3(c)).



Fig. 2. Asiaticoside yields extracted from Centella asiatica (L.) by [TEA][HSO4] /EtOH = 1 g/ml at 65 °C. (NS (non-significant): p greater than 0.05) and \*p < 0.05(significant).

#### Table 2

Experimental design parameters and output.

RUN	Independent variable	S	Dependent variables				
	X1:	X <sub>2</sub> :	X <sub>3</sub> :	Y1:	Y <sub>2</sub> :	Y <sub>3</sub> :	
	Temperature (°C)	Extraction time (Hours)	[TEA][HSO <sub>4</sub> ] %	AY (%,w/w)	TPC (mg GAE /g)	TEAC (µmolTE/g)	
1	55	24	40	3.55 ± 0.030	60.84 ± 0.00	40.04 ± 1.69	
2	30	24	20	$3.52 \pm 0.040$	66.57 ± 16.24	61.88 ± 2.28	
3	55	12	40	$4.44 \pm 0.030$	68.98 ± 0.00	56.36 ± 0.00	
4	30	24	60	2.75 ± 0.015	32.47 ± 0.00	29.28 ± 0.00	
5	80	12	60	4.27 ± 0.017	50.60 ± 1.64	48.67 ± 13.90	
6	30	18	40	3.96 ± 0.013	57.00 ± 2.47	50.07 ± 2.63	
7	55	18	40	4.43 ± 0.005	75.95 ± 0.00	63.76 ± 3.02	
8	55	18	40	$4.29 \pm 0.009$	71.88 ± 6.74	53.50 ± 0.00	
9	55	18	40	4.27 ± 0.002	88.28 ± 0.99	53.50 ± 0.00	
10	80	24	60	3.57 ± 0.032	34.56 ± 0.00	36.60 ± 0.00	
11	30	12	20	3.87 ± 0.010	111.30 ± 21.05	66.64 ± 0.35	
12	55	18	20	4.00 ± 0.033	112.58 ± 26.80	72.05 ± 0.00	
13	80	24	20	3.92 ± 0.001	18.98 ± 1.97	50.41 ± 0.00	
14	55	18	40	4.34 ± 0.046	91.19 ± 0.16	59.38 ± 0.00	
15	55	18	40	4.04 ± 0.011	82.35 ± 1.81	65.41 ± 0.00	
16	80	12	20	4.75 ± 0.030	89.44 ± 0.00	66.97 ± 9.49	
17	30	12	60	3.01 ± 0.019	25.72 ± 0.00	31.28 ± 0.00	
18	55	18	40	4.32 ± 0.020	77.23 ± 3.12	58.43 ± 5.83	
19	80	18	40	$4.54 \pm 0.003$	55.02 ± 0.00	50.26 ± 2.91	
20	55	18	60	2.97 ± 0.023	57.58 ± 8.22	36.33 ± 0.38	

#### Table 3

Multiple regression analysis and model equations fitted for all responses.

Responses	Model Equation	Model Significant	Lack-of-fit Test	R <sup>2</sup>
	+4.20 + 0.3931 X <sub>2</sub> -0.3031 X <sub>2</sub> -0.3486 X <sub>2</sub> + 0.1676 $X_2^2$ -0.0901 $X_2^2$	<0.0001 (Significant)	0.1118(not significant)	0.9384
AY	$- 0.5981 X_3^2 - 0.1155 X_1 X_2 + 0.0999 X_1 X_3 + 0.0276 X_2 X_3$			Adjusted 0.8830
				Predicted 0.6940
	+79.694.45 X <sub>1</sub> -13.26 X <sub>2</sub> -19.80 X <sub>3</sub> -21.50 X <sub>1</sub> <sup>2</sup> - 12.61 X <sub>2</sub> <sup>2</sup> + 7.57 X <sub>3</sub> <sup>2</sup> -6.06 X <sub>1</sub> X <sub>2</sub> + 12.05 X <sub>1</sub> X <sub>3</sub> + 13.25 X <sub>2</sub> X <sub>3</sub>	< 0.0001 (Significant)	0.3229 (not significant)	0.9447
TPC				Adjusted 0.8948
TEAC	+56.90 + 1.38 X <sub>1</sub> –5.17 X <sub>2</sub> –13.58 X <sub>3</sub> –3.59 X <sub>1</sub> <sup>2</sup> –5.56X <sub>2</sub> <sup>2</sup> + 0.43 X <sub>3</sub> <sup>2</sup> –2.73 X <sub>1</sub> X <sub>2</sub> + 4.48 X <sub>1</sub> X <sub>3</sub> + 0.91X <sub>2</sub> X <sub>3</sub>	0.0006	0.3876 (not significant)	Predicted 0.7221 0.9028
		(orginiteant)		Adjusted 0.8153
				Predicted 0.6258

#### Table 4

Analysis of variance (ANOVA) for all responses.

AY (%, w/w)		TPC (mg GAE/g)			TEAC (μmol TE/g)				
Variables	Coefficient	F	Prob > F	Coefficient	F	Prob > F	Coefficient	F	Prob > F
X <sub>1</sub> -temperature	0.3931	43.03	< 0.0001	-4.45	2.77	0.1269	1.38	0.66	0.4361
X <sub>2</sub> -extraction time	-0.3031	25.58	0.0005	-13.26	24.58	0.0006	-5.17	9.29	0.0123
X <sub>3</sub> -[TEA][HSO <sub>4</sub> ] %	-0.3486	33.83	0.0002	-19.80	54.83	< 0.0001	-13.58	64.05	< 0.0001
Interaction									
$X_1X_2$	-0.1155	2.97	0.1155	-6.06	4.10	0.0703	-2.73	2.08	0.1801
X <sub>1</sub> X <sub>3</sub>	0.0999	2.22	0.1668	12.05	16.23	0.0024	4.48	5.58	0.0398
X <sub>2</sub> X <sub>3</sub>	0.0276	0.17	0.6885	13.25	19.63	0.0013	0.91	0.23	0.6431

#### 3.4. Role of [TEA][HSO<sub>4</sub>]

Generally, bioactive compounds are secluded in rigid, thick cell walls containing polysaccharides as the major components. Hence,

any extraction techniques should be able to make the cell walls permeable, permitting the bioactive emission from the cells.

We obtained low AY when we first performed ethanolic extraction (EtOH-40%) at 65  $^{\circ}$ C for 1 h. These suggest minimal destruc-



Fig. 3. Three-dimensional surface of (a) TPC: extraction time - [TEA][HSO4]%; (b) TPC: temperature - [TEA][HSO4]%, and; (c) TEAC: temperature -[TEA][HSO4]%.

tion of cell walls by ethanolic extraction. Interestingly, adding [TEA][HSO<sub>4</sub>] as the co-solvent enhanced asiaticoside yield by nine times. We associate this with the intensified destruction of cell walls caused by  $[H_3O]^+$  ions, which arose from  $H_2O$  molecules protonation by the acidic protons of  $[HSO_4]^-$  ions during the extraction process (Roy et al., 2020).

Regarding TPC and subsequent TEAC, the release of phenolic compounds appeared to increase with the temperature at a fixed [TEA][HSO<sub>4</sub>]%. Higher temperatures lead to H<sub>2</sub>O molecules protonation increment, generating more  $[H_3O]^+$  ions that further intensify the destruction of cell walls.

#### 3.5. Validation of the predictive model

The optimal C. asiatica extraction was 66 °C, 12 h, and 20% [TEA] [HSO<sub>4</sub>] at predicted AY of 4.39% (w/w), TPC of 112.58 mg GAE /g, and TEAC of 70.62  $\mu$ mol TE/g respectively. At the same time, the experimental data at optimum conditions were 4.44 ± 0.05% (w/w), 114.11 ± 12.58 mg GAE/g, and 70.01 ± 5.74  $\mu$ mol TE/g. The experimental and predicted value proximity confirms the practicability of optimum conditions.

Interestingly, the results above were far higher than those reported in previous studies. The asiaticoside yield obtained was ca. 3.40%, 3.29%, and 4.27% higher than reported (Table 5). Simi-

#### Table 5

Asiaticoside yield, TPC, and TEAC in previously reported studies.

Extraction conditions	Asiaticoside yield (%,w/w)	TPC (mg GAE/g)	TEAC (μmol TE/g)
MAE:40% EtOH, 153 W, 10 min (Thong-On et al., 2021)	1.031	-	-
UAE: 40% EtOH, 55 °C, 90 min (Thong-On et al., 2021)	1.155	-	-
95% EtOH, 60 °C, 120 min (Monton et al., 2019)	0.174	-	-
40% EtOH, 65 °C, 60 min (Chew et al., 2011)	-	12.03	19.48

larly, TPC and TEAC were markedly increased by 89% and 72%, respectively, compared to previous studies (Table 5).

#### 4. Conclusion

Triethylammonium hydrogen sulfate, [TEA]HSO<sub>4</sub>] mediated cosolvent able to enhance asiaticoside extraction. At optimal conditions of 66 °C, 12 h, and 20% [TEA]HSO<sub>4</sub>], the yield of asiaticoside, TPC, and TEAC were  $4.44 \pm 0.05\%$  (w/w), 114.11 ± 12.58 mg GAE /g, and 70.01 ± 5.74 µmol TE/g respectively. All responses fit the quadratic model, and the optimal conditions can be applied practically for efficient C. asiatica extraction. The outcomes of this research, give an overview of PILs potential as bioactive extractants, besides widening the application of other PILs toward plant extraction. The extract's high antioxidant capacity will be beneficial in plant-based product development. Research expansion comprising the solute– solvent interaction will be beneficial in designing more efficient plant extraction and broadening the plant-based product market.

#### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### Acknowledgments

The authors appreciate the financial support under grant FRGS/1/2019/STG01/UKM/02/12 and GUP-2017-014. Shikh Zahari also extends appreciation to the Ministry of Higher Education of Malaysia (MOHE) for scholarship awards (KPT(BS)860407335591) as a postdoctoral research fellow at Imperial College London, UK.

#### **Appendix A. Supplementary material**

Supplementary data to this article can be found online at https://doi.org/10.1016/j.jksus.2023.102863.

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